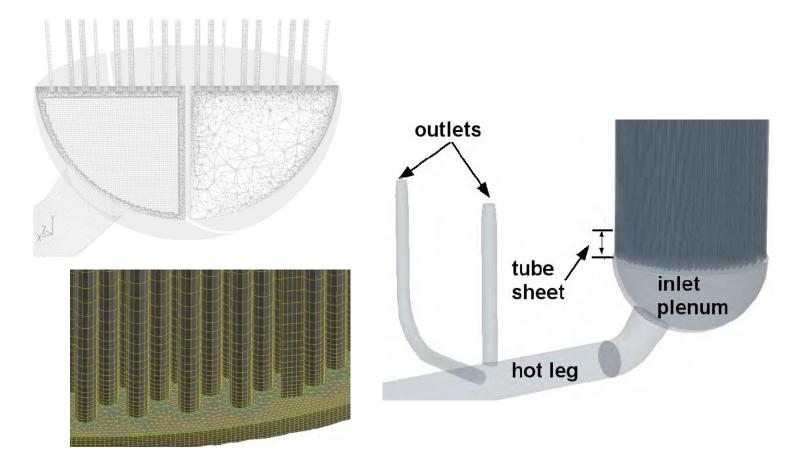


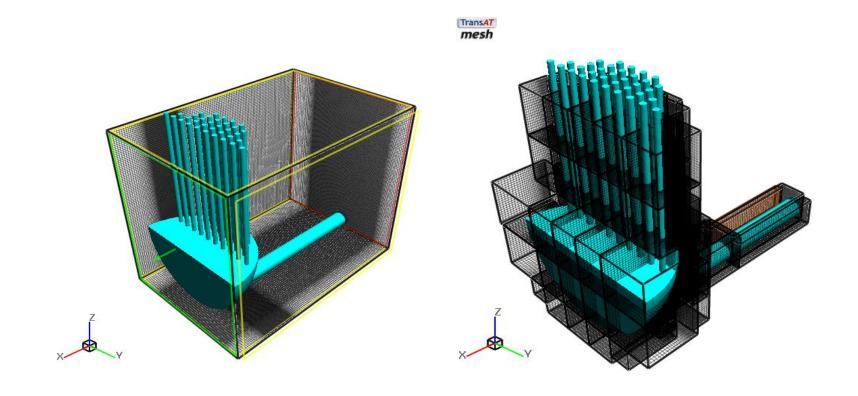
Flow in Steam Generators: Fluent grid



Courtesy: NRC (Chris Boyd, FLUENT)



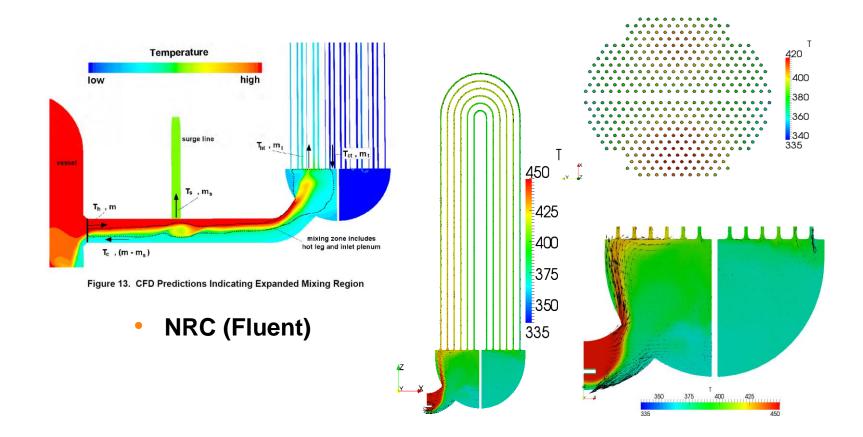
Flow in Steam Generators: TransAT grid



ASCOMP (TransAT)



Fluent & TransAT solutions

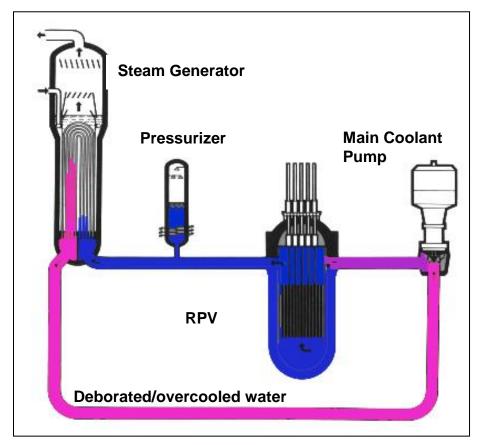


ASCOMP (TransAT)



Boron mixing in PWR primary circuit

- PWR is equipped with 2 or more loops (German KONVOI: 4)
- Boron dissolved in the coolant acts as neutron absorber
- Hypothetical accidents with creation of lower borated slugs in single loops
- Importance of mixing of coolant with different boron content

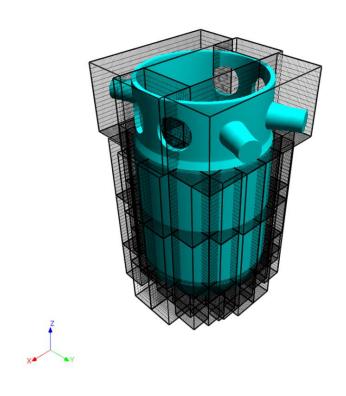


Primary circuit of a PWR

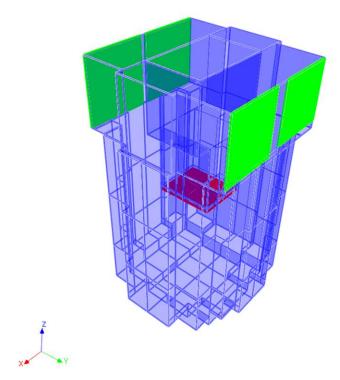
ROCOM tests (SIEMENS Germany)



Boron dilution: 1D-3D Coupling (Cathare-transat)



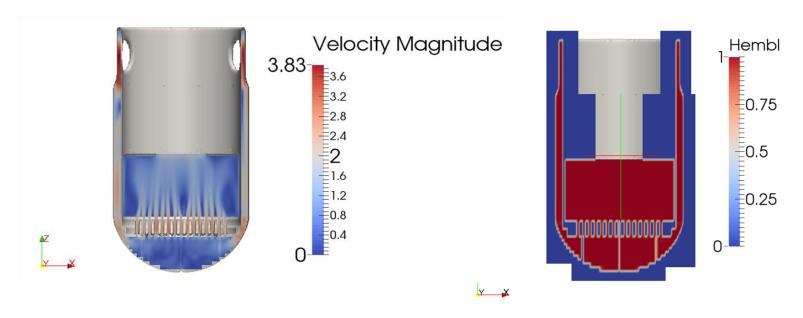
- The flow is simulated with TransAT.
- The fluid domain is shown in blue everything else is solid ("inverted" view).
- IST mesh is created by using multiple blocks with a total of 700k cells.



- The inlet boundaries, indicated by green surfaces, have velocity = 2.91m/s
- The outlet/coupling boundary is indicated by a red surface, with no prescribed conditions.



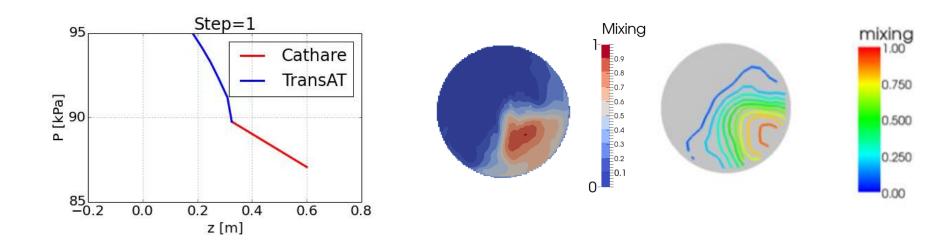
Boron dilution: 1D-3D Coupling (cathare-transat)



- Planes are perpendicular to the Y direction
- Fluid goes deep into the lower plenum, and then rises up through the support plate.
- Sharp interface is implemented, which creates gaps between adjacent objects. The unexpected gaps in the lower plenum will affect the fluid field.



Boron dilution: 1D-3D Coupling (cathare-transat)



- With a larger time step, there are no significant pressure oscillations in CATHARE.
- At the coupling interface, pressure values from both sides match well.

- The maximum mixing scalar is very well captured by the coupled solution.
- The concentration spreading is only slightly underestimated compared to the data.

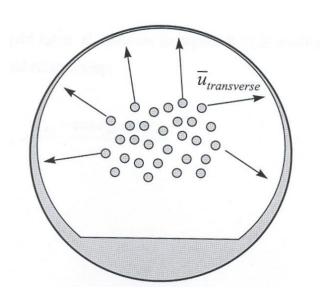


Droplet entrainment: The practical context

Air-water flow



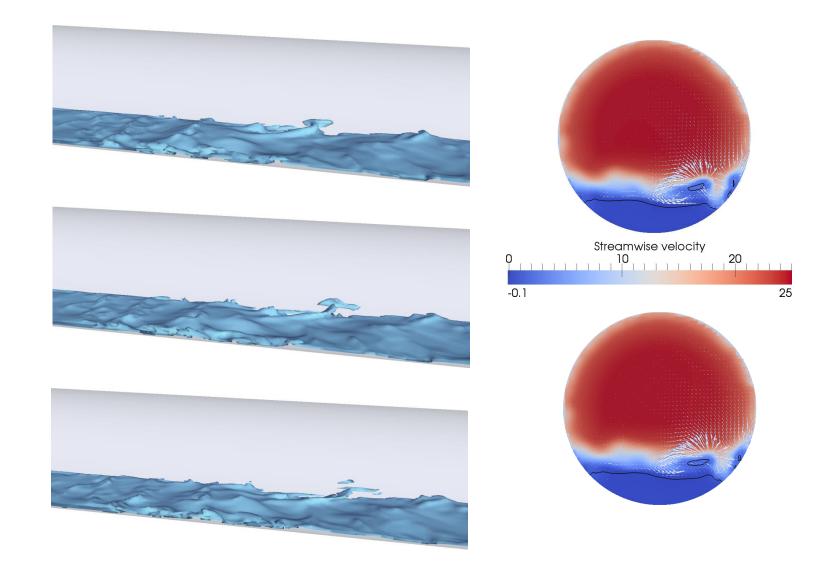
Wetting mechanism



Courtesy: Badie & Hewitt © Imperial College London

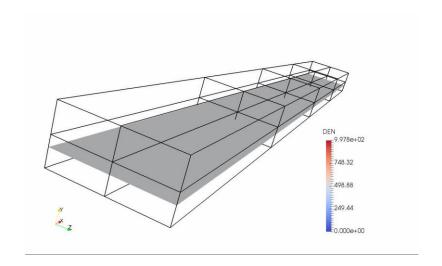


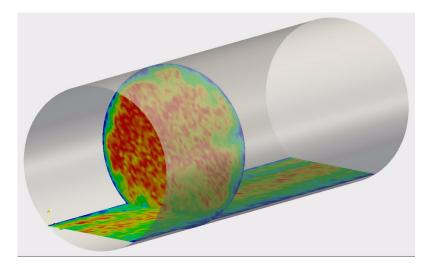
LEIS of droplet entrainment in a pipe

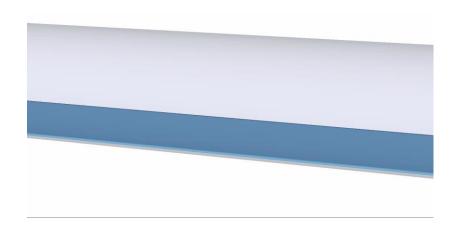


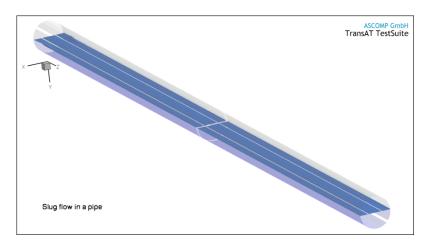


Free-surface horizontal flows









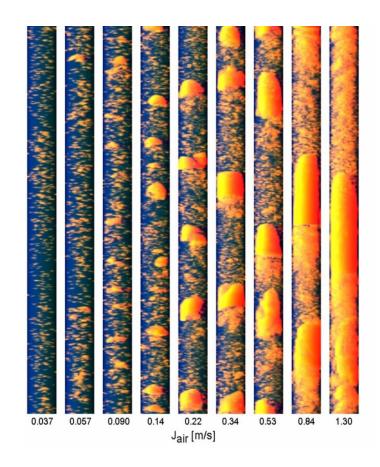


Vertical Flow: The Issues

- Flow regime map definition (e.g. slug speeds & size, etc.)
- Phase distribution
- Pressure drop and thermal transients
- Large diameter risers.

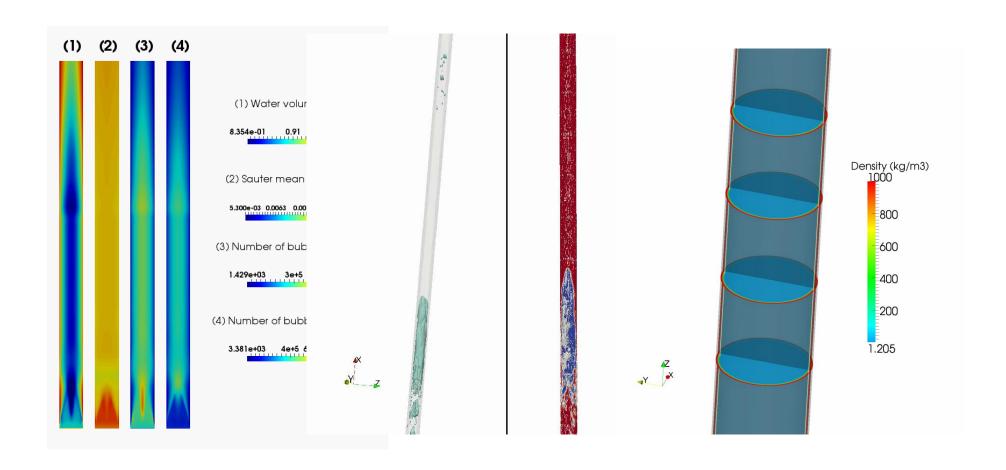
Why CMFD?

- Can simulate various flow regimes.
- Advanced models (ITM) are needed for certain flow patterns (e.g. slugging), and
- Can help identify flow regimes for large-diameter risers, as
- Shown in examples of next slide.



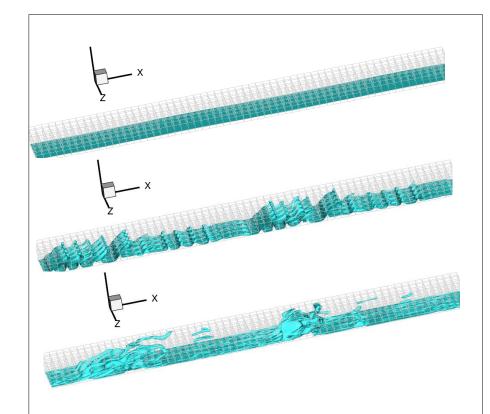


Flow Regime Prediction

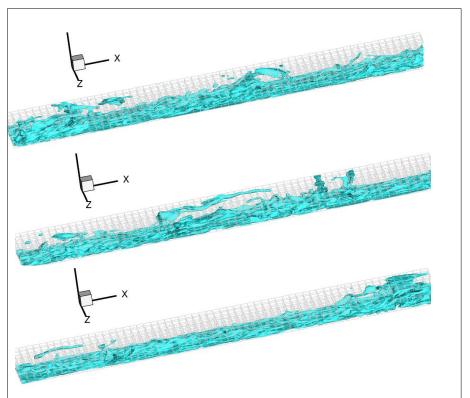




Annular Flow (full domain)



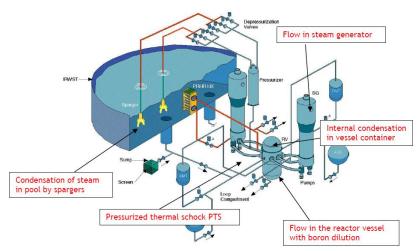
- $J_g = 20$ m/s, $J_l = 1.5$ m/s. Comp. domain spans one full wavelength
- LEIS: Total number of grid points is 10 million cells distributed over 960 cores.



- Ligament formation, droplet detachment, formation of large disturbance wave clearly visible in these simulations
- Flow for full domain still developing.

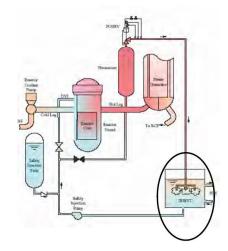


Condensation of steam jets from a sparger in a pool (KEPCO Korea)



Tangential velocity magnitude
0.003644
1.534903

Figure 1: AP1000 RCS and passive core cooling system (Schulz, 2006)







Condensation of steam jets from a sparger in a pool (KEPCO Korea)

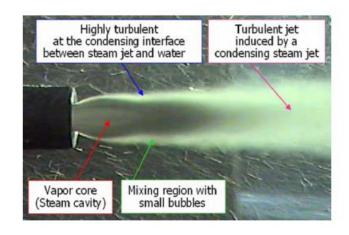
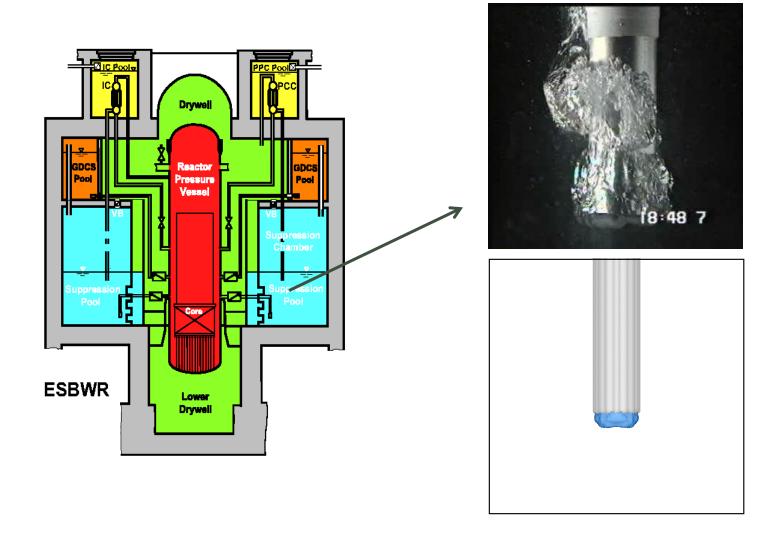


Image of condensing jet from Song et al. (2012)



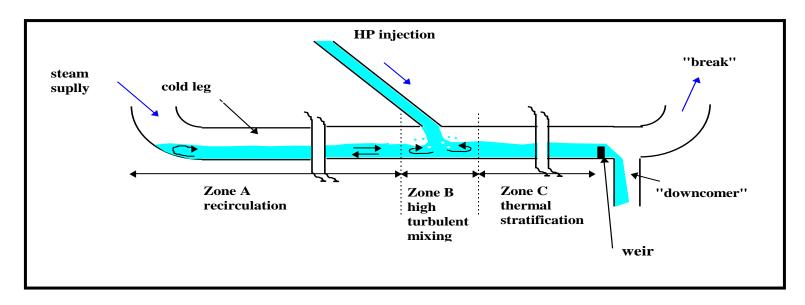


RPV de-pressurisation





PTS: COSI Exp. (AREVA)

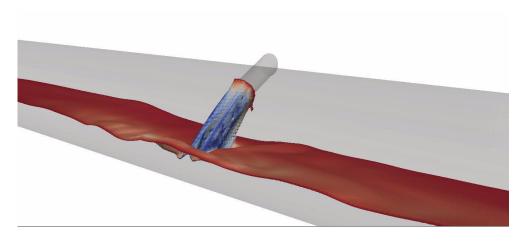


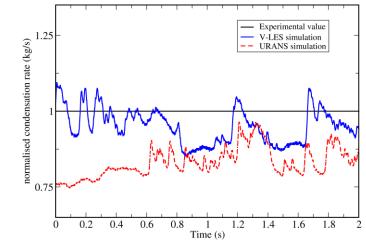
- Courtesy from Yadigaroglu and Bestion, ICAPP07
- During a hypothetical SB-LOCA, cold water is injected into the cold leg to limit the RPV lifetime (Emergency Core Cooling, ECC).
- The injected water mixes with the hot fluid in the cold leg and flows towards the downcomer leading to excessive thermal stresses on the RPV walls.



Rate of condensation

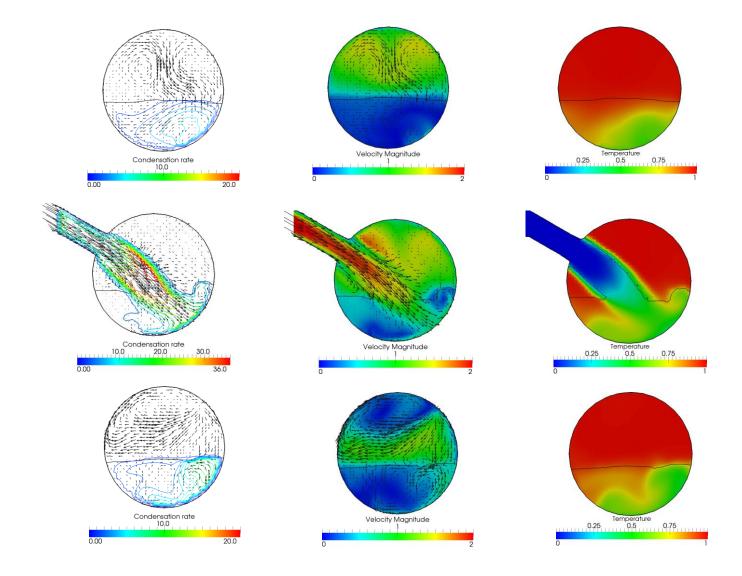
- ECC injection of cold water (296 K) in saturated water
- Steam at saturation temperature (485 K)
- Pressure 20 bars
- Simulation with TransAT level-set technique
- RANS vs. V-LES models for turbulence
- Interfacial condensation model (Labois & Lakehal, 2010)





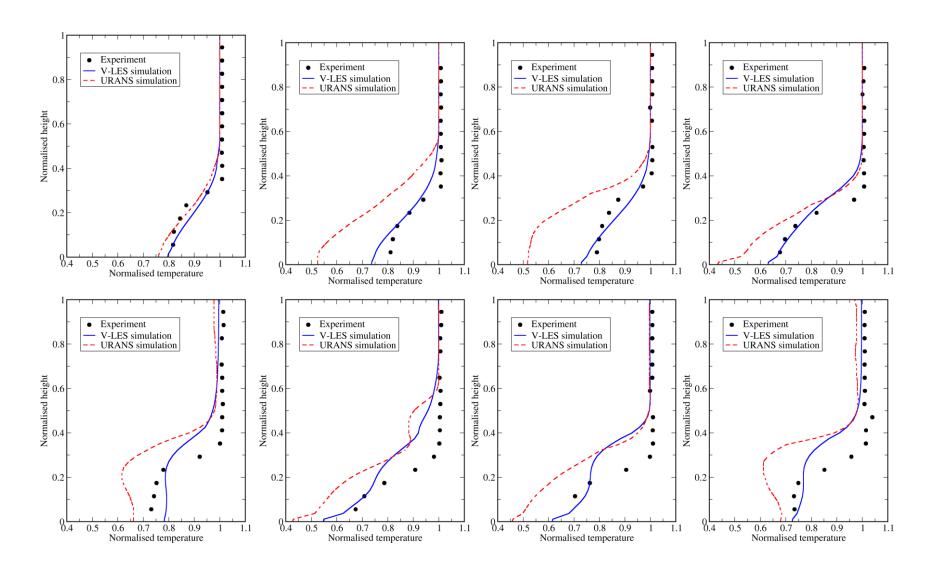


Cross-section interface & temperature



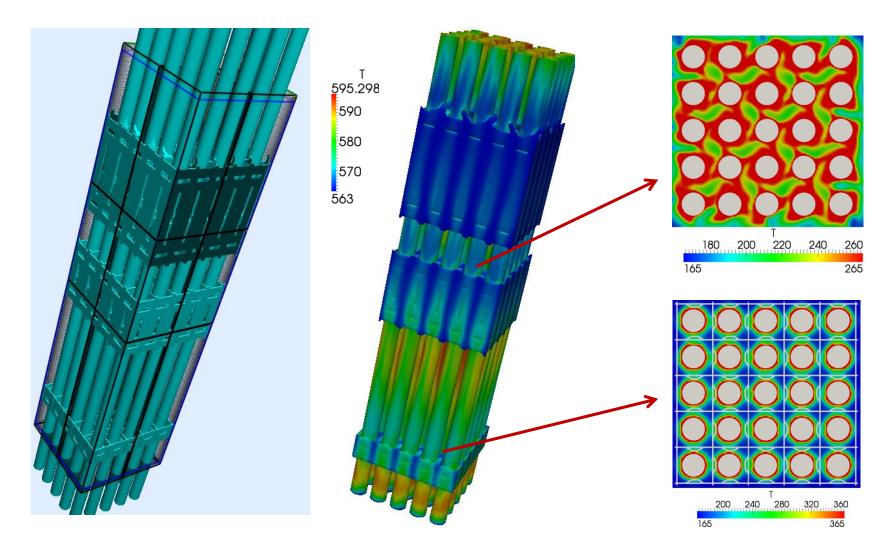


Temperature average results





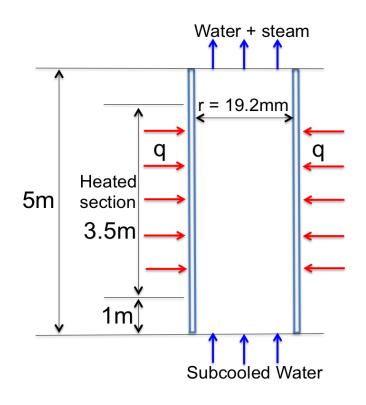
The OECD PSBT 5x5 Benchmark 20





Bubbly-flow boiling: Debora test case (CEA)

DEBORA EXPERIMENTS OF MANON ET AL (2000, 2001)



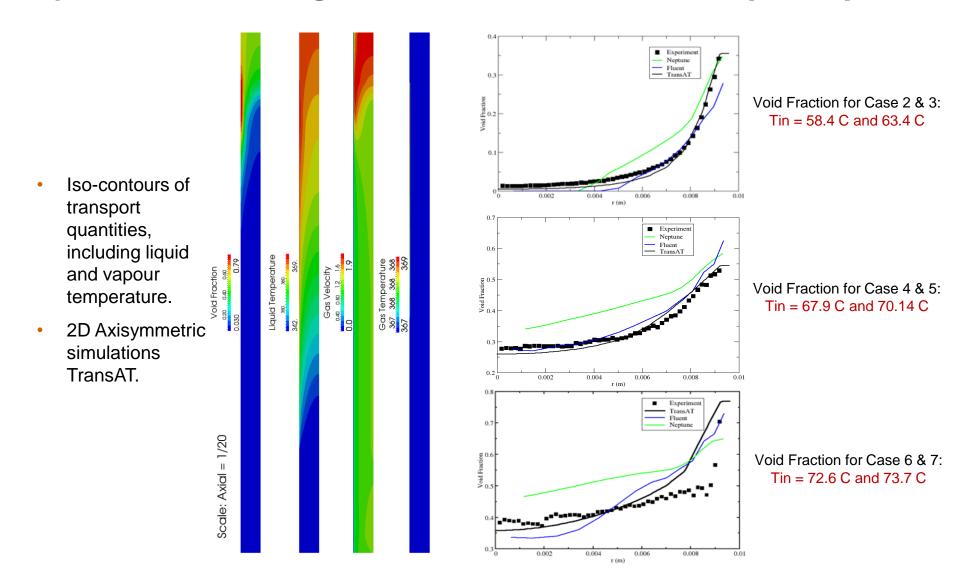
Pipe Length: 5m

Pipe Diameter: 19.2 mm

Case	mass flux	T _{inlet}	T_{sat}	Bubble dia
No.	kg/m ² /s	°C	°C	mm
1	1006.8	52.97	94.136	0.2
2	1007.4	58.39	94.136	0.58
3	999.5	63.43	94.136	0.65
4	1005	67.89	94.136	3.2
5	1004.8	70.14	94.136	4.0
6	1004.8	72.65	94.136	5.1
7	994.9	73.7	94.136	6.2



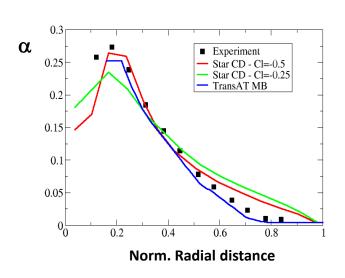
Bubbly-flow boiling: Debora test case (CEA)

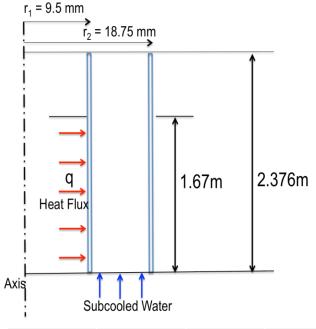




Bubbly-flow boiling: Lee et al. & Tu & Yeoh (KAERI)

EXPERIMENTS OF LEE, PARK & LEE (2002) AND TU & YEOH (2003)



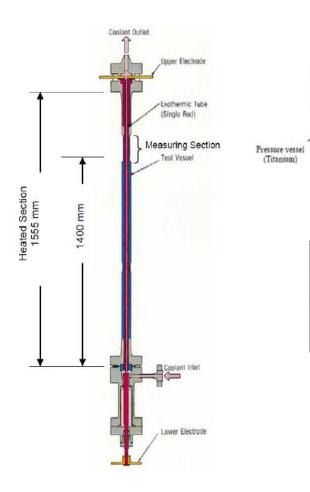


- Pipe Length: 2.376m
- *q*=152.3 kW/m²
- G_{\parallel} =474 kg/(m²s)
- *P*=0.14 Mpa
- $\Delta T_{sub} = 11.5 \text{ K}.$

Heat flux	mass flux	T inlet	T _{sat}
MW/ m²	kg/m²/s	K	K
0.1523	474	371.5	383



NUPEC PWR Test Facility



Testcas e	Pressur e [MPa]	Inlet Tem p [°C]	Powe r [kW]	Mass Flux [kg m ⁻² s ⁻
1.2211	15	295.4	90	11
1.2223	15	319.6	70	11
1.2237	15	329.6	60	11
1.4411	10	238.9	60	5
1.4325	10	253.8	60	2
1.4326	10	268.8	60	5
Cell	No o	f	No	Wall

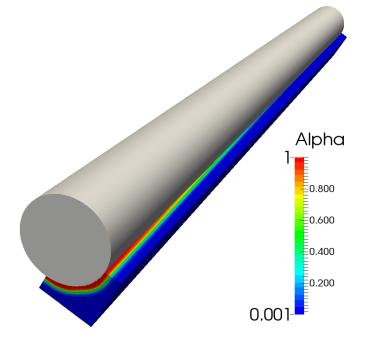
(Alumina)

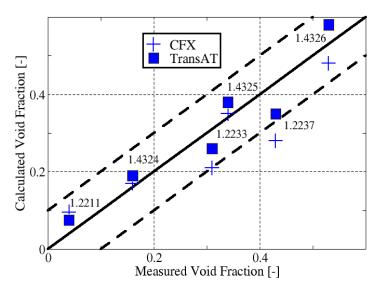
Cell Size (in mm)	No. of Cells	No. of Proces sors	Wall Clock Time (in days)
5.31	9216	1	0.33
2.655	73728	8	0.75
1.328	1280000	108	1.5
0.885	2880000	128	4



NUPEC PWR Test Facility

- Iso-contours of vapour void fraction.
- Calculated vs. measured space-averaged void fraction.
- Comparison with CFX results

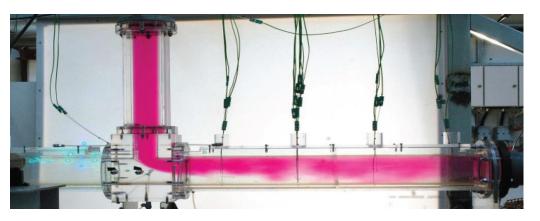


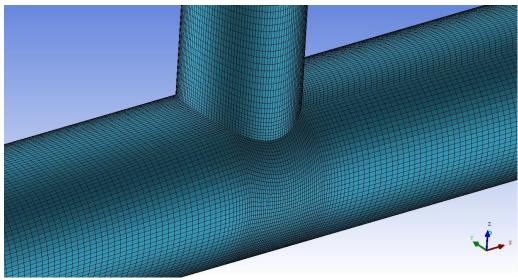




LES of Thermal stipping in a T-junction

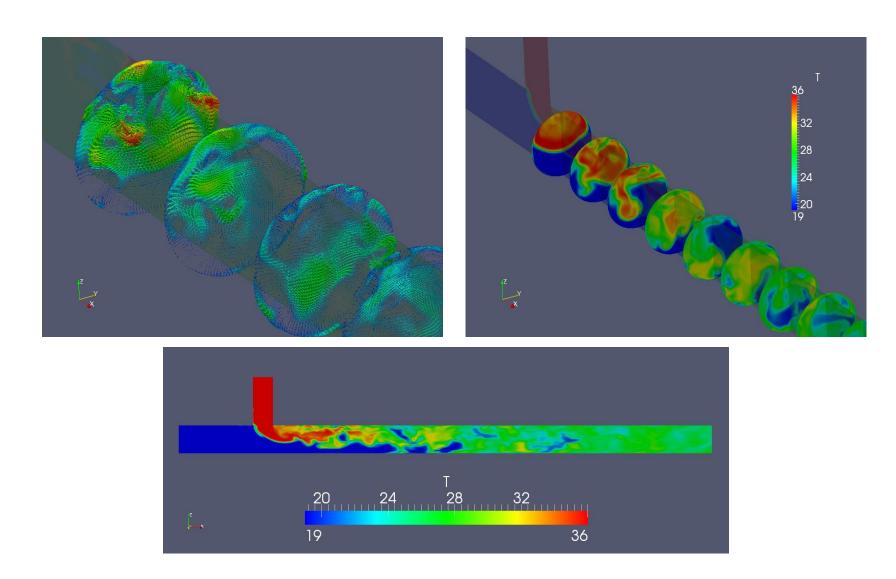
- Flow visualization test in the Vattenfall T-junction test facility (Älvkarleby Labs., Vattenfall R&D).
- Re = 1.9E5; ΔT = 15 Deg.
- BFC grid (3 million cells)
- LES with WALE SGS model





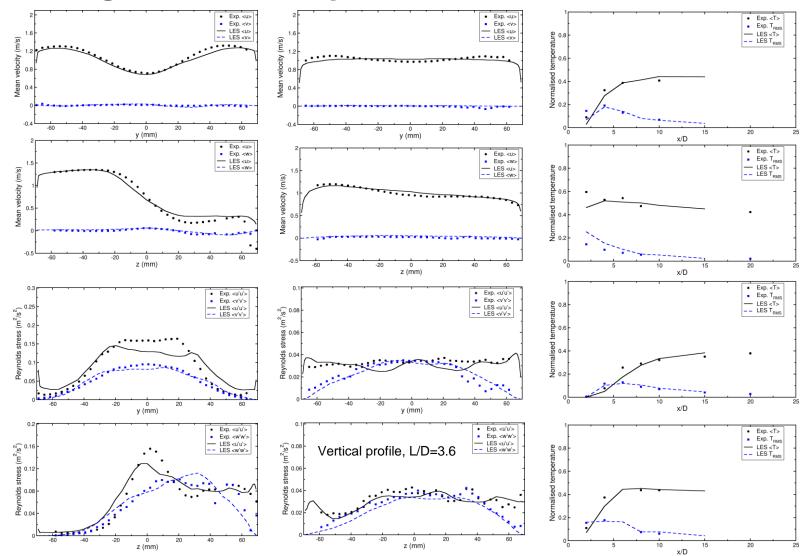


Instantaneous results





Time average results (mean & r.m.s variables)

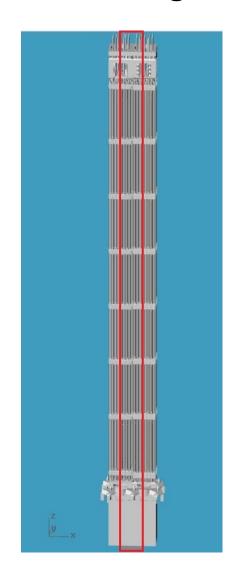


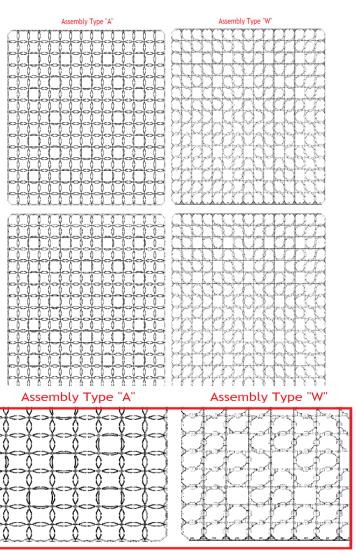


Grand-challenge problem



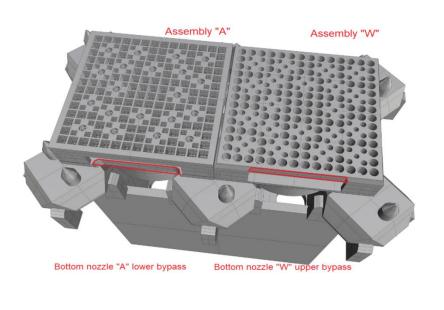
Convective boiling flow in two types of assemblies

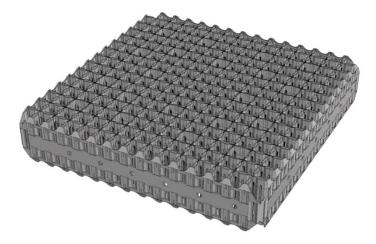


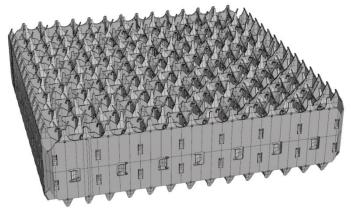


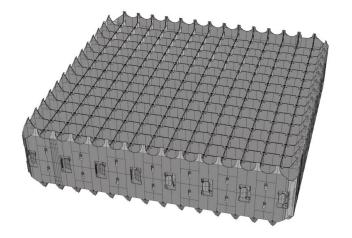
Two assembly types and the min simulation domain (in red)





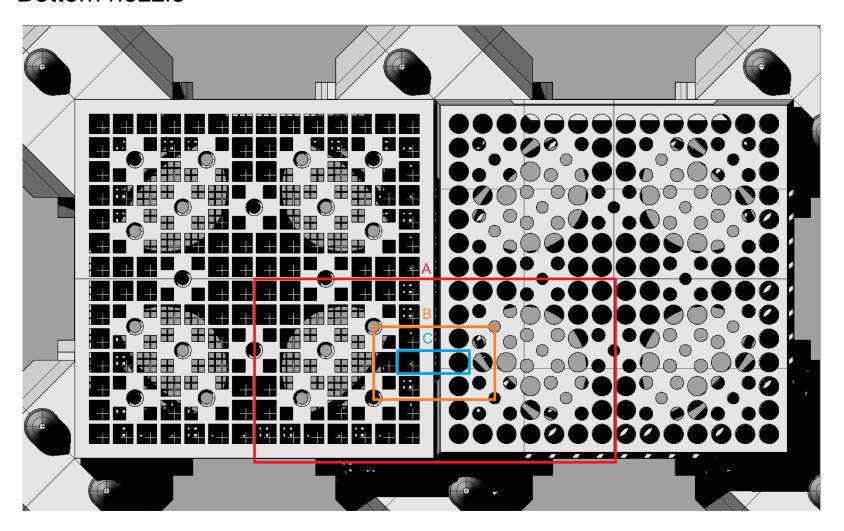








Bottom nozzle

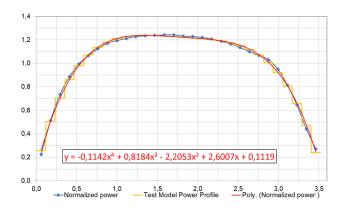




Parameter	Value
Reactor Power [MWth]	3002
Average Linear Power [W/cm]	235.04
Coolant Inlet Temperature [K]	564.65
Coolant Outlet Average Temperature [K]	599.35
System Pressure [bar]	154
Core mass flow rate [kg/s]	15980
Core volumetric flow rate [m³/s]	21.502
Total core total bypass, mass flow rate [kg/s]	749.46 (=4.69% of core mass flow rate)
Bypass through thimble tubes, m. flow rate [kg/s]	263.67 (=1.65% of core mass flow rate)

367,1	371,4	395,9	0,0	403,4	382,5	373,6	376,6		
371,4	378,1	389,9	411,5	402,6	406,6	384,3	379,2		
395,9	389,9	396,3	417,5	422,8	0,0	403,6	383,5		
0,0	411,5	417,5	0,0	423,7	414,3	389,5	382,8		
403,4	402,6	422,8	423,7	404,2	408,6	385,5	379,2		
382,5	406,6	0,0	414,3	408,6	0,0	392,6	374,0		
373,6	384,3	403,6	389,5	385,5	392,6	368,1	364,9		
373,6	379,2	383,5	382,8	379,2	374,0	364,9	358,7		
8	7	6	5	4	3	2	1		
			Assen	nbly A					

376,6	373,6	382,5	403,4	0,0	395,9	371,4	367,1
379,2	384,3	406,6	402,6	411,5	389,9	378,1	371,4
383,5	403,6	0,0	422,8	417,5	396,3	389,9	395,9
382,8	389,5	414,3	423,7	0,0	417,5	411,5	0,0
379,2	385,5	408,6	404,2	423,7	422,8	402,6	403,4
374,0	392,6	0,0	408,6	414,3	0,0	406,6	382,5
364,9	368,1	392,6	385,5	389,5	403,6	384,3	373,6
358,7	364,9	374,0	379,2	382,8	383,5	379,2	373,6
1	2	3	4	5	6	7	8



Assembly A

Quarter average assembly power distribution [W/cm] for both assembly

Axial power distribution and fitted shape function



	Axial Coordinate [mm]					AR	
	Z _{start}	Z _{end}	Δz	[mm]			
Domain extention and Bott. plate	-50	385	385	435	0.25	10	
Bottom nozzle lower part	385	554	604	169	0.25	10	1
Bottom nozzle filter and bottom spacers	554	742	792	188	0.25	1	4.470
Rods	742	1120	1170	378	0.25	10	1170 4.362E+08
Guide tube hole	1120	1212	1262	92	0.25	1	2
2 nd spacers	1212	1306	1356	94	0.25	1	_
Rods	1306	1673	1723	367	0.25	10	553 3.366E+08
Rods	1673	1746	1796	73	0.25	10	3
3 rd Spacers and sleeves	1746	1839	1889	93	0.25	1	Ŭ
Rods	1839	2207	2257	368	0.25	10	534 2.142E+08
Rods	2207	2280	2330	73	0.25	10	4
4 th Spacers and sleeves	2280	2373	2423	93	0.25	1	7
Rods	2373	2740	2790	367	0.25	10	533 2.144E+08
Rods	2740	2813	2863	73	0.25	10	5
5 th Spacers and sleeves	2813	2907	2957	94	0.25	1	
Rods	2907	3275	3325	368	0.25	10	535 2.147E+08
Rods	3275	3346	3396	71	0.25	10	6
6th Spacers and sleeves	3346	3441	3491	95	0.25	1	
Rods	3441	3808	3858	367	0.25	10	533 2.144E+08
Rods	3808	3879	3929	71	0.25	10	7
7 th Spacers and sleeves	3879	3972	4022	93	0.25	1	·
Rods	3972	4335	4385	363	0.25	10	527 2.136E+08
Rods	4335	4403	4453	68	0.25	10	8
8 th Spacers and sleeves	4403	4512	4562	109	0.25	1	J
Region above rods up to guide tubes end plug	4512	4570	4620	58	0.25	1	665
Top nozzle and upper plate	4570	4753	4803	183	0.25	10	
Upper plate and domain extention	4753	5000	5000	247	0.25	10	3.329E+08
			Total	5050	-	-	2.177E+09
		Total fin	e meshing	859	0.25	1	1.278E+09
				4191	0.25	10	8.993E+08



